

# Towards Data-Driven NARX ANN Simulation for Optimal Control of the Flue Gas Desulphurization for Coal Power Plants

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## KEYWORDS

$SO_X$  absorption, data-driven modeling, and simulation, semi-dry gas desulfurization, optimal control, artificial neural network

## ABSTRACT

This paper presents the ANN-based algorithm for data-driven optimal control of desulfurization of the flue gases from Coal Power Plants. We have proposed the NARX recurrent neural network with experimentally selected feedback connection length as the black box model for the first stage of the control process. Then simple brute force algorithm was used to find the optimal level of the reagent added into the system to keep the  $SO_X$  concentration outlet below the assumed level. This procedure was designed for a known level of  $SO_X$  concentration inlet. The proposed approach was tested on real data collected from the selected Coal Power Plant in Poland. The simulation that was made confirms that such an approach is effective for coal power plants to increase their energy efficiency and meet the appropriate environmental standards.

## I. INTRODUCTION

Sulfur oxides pollute the air and have a negative impact on human health [1] and ecosystems [2]. Desulfurization of flue gases with  $SO_X$  ( $SO_2$  and  $SO_3$ ) emissions is one of the main challenges for the energy industry. The main source of sulfur dioxide emissions is the combustion of coal for energy production. In Poland, half of the  $SO_X$  emissions are attributed to the energy industry (according to the national report [3]). The reduction in the amount of  $SO_X$  emissions is linked to Poland's accession to the European Union and compliance with the Industrial Emissions Directive on emission limits. Current standards allow emissions from flue gas desulfurization plants at  $200 \text{ mg/Nm}^3$ .

This study aimed to develop a nonlinear autoregressive exogenous Neural Network model (NARX ANN) learned from industrial field data of the process of semi-dry flue gas desulphurization with soft-burned quicklime. The required quantity of reagent (CaO) for the purification of sulfur discharges produced by a Coal Power Plant was forecasted. Our objective pertains

to the enhancement of technological processes with the aim of optimizing reagent consumption, which leads to a reduction in own costs but also affects the protection of the environment.

## II. PROBLEM FORMULATION

The control problem for the flue gas desulfurization is based on the fact that  $SO_X$  emissions depend on two factors: the level of  $SO_X$  concentration inlet and the amount of the reagent added to the working system, see tab. 1, and fig. 1. The more reagents added the less  $SO_X$  concentration outlet is produced. However, adding more reagents results in an increase in the cost of the process. Moreover, the  $SO_X$  concentration outlet must be kept below a certain level, given by international norms and standards. Optimal Control of the Flue Gas Desulphurization for Coal Power Plants may be formulated as follows:

- $SO_X$  concentration outlet(reagent amount) <  $SO_X$  concentration outlet critical value;
- reagent amount  $\rightarrow$  min.

For solving this problem data-driven approach was adopted. It does not require modeling the system using closed mathematical formulas. Instead, ANN (artificial neural network) was used as the black-box model for the dependence between  $SO_X$  concentration outlet,  $SO_X$  concentration inlet, and reagent amount. ANN was trained to predict the level of  $SO_X$  concentration outlet (ANN targets) based on reagent amount  $SO_X$  (first element of ANN input) and  $SO_X$  concentration inlet (first element of ANN input).

Data	variable name
reagent	$input_{ca}$
$SO_X$ concentration inlet	$input_s$
$SO_X$ concentration outlet	$output_{so2}$

TABLE 1: Considered data description and variables used in Matlab simulation

The next stage is to use the trained ANN as the black box model for the simulation of the working system and

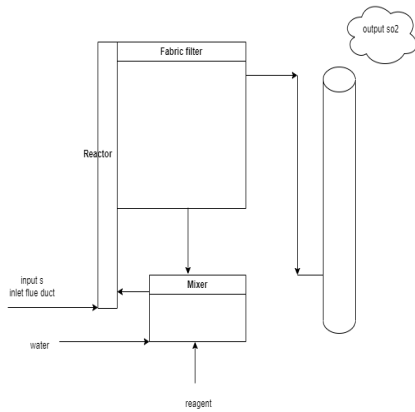


Fig. 1: Flue Gas Desulphurization for Coal Power Plants schema

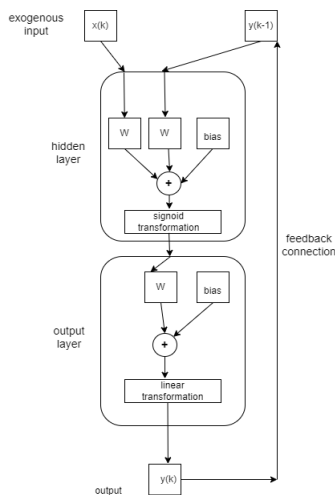


Fig. 2: The nonlinear autoregressive network with exogenous inputs (NARX), a recurrent dynamic network, with feedback connections enclosing several layers of the network

the prediction of the amount of the reagent for the given level of  $SO_X$  concentration inlet. The aim is to determine the impact of different reagent amounts on the level of a  $SO_X$  concentration outlet. Based on those simulations, the system may be controlled for the next stage of operation. For this aim, the nonlinear autoregressive network with exogenous inputs (NARX), see fig. 2, a recurrent dynamic network with feedback connections enclosing output and input layers, was used, [4]. Such ANN is reported to obtain very good results in time-series modeling. To verify the quality of modeling, the mean squared error (MSE) and R coefficient of variation were used for the learning and testing process separately, [5]:

$$MSE = \sum_{k=1, \dots, K} (ANN_{target}(k) - ANN_{output}(k))^2 / K \quad (1)$$

and the *meanErr*, the mean absolute of the testing

errors obtained from the testing process:

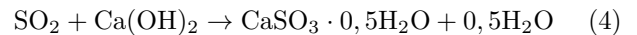
$$meanErr = \quad (2)$$

$$mean_{k=1, \dots, K} |ANN_{target}(k) - ANN_{output}(k)| \quad (3)$$

where  $k = 1, \dots, K$  denotes the  $k$ th sample from the training/validation/testing set.

### III. RELATED WORK

There are several methods using different absorbents to flue gas desulfurization, of which the most popular is limestone for economic reasons [6]. Taking into account the sorbent dosing method, as well as the reception of the product formed during flue gas desulfurization, calcium-based methods are classified as dry, semi-dry, and wet. These methods use the reaction between calcium oxide and sulfur dioxide to reduce  $SO_X$  emissions [7]. The industrial process that combines CaO to reduce pollutant emissions from the Coal Power Plant is described below. Acidic pollutants from flue gases are removed by introducing hydrated or burnt lime  $Ca(OH)_2$ . This lime reacts with sulfur dioxide ( $SO_2$ ) and hydrogen chloride (HCl) to form hydrated calcium sulfate ( $CaSO_3$ ) and calcium chloride ( $CaCl_2$ ), which are then transported by the gas flow:



Dry and semi-dry methods produce desulfurization product in a dry state, called End Product. In semi-dry methods, the temperature has a significant impact on the product state. Wet methods result in a suspension or slurry. Due to its higher efficiency and lower costs, the semi-dry method is the most commonly used in the energy industry [8]. At the same time, the effectiveness of  $SO_X$  removal is complex and depends on many factors. The reactivity of the calcium-based sorbent is variable. The process, as an exothermic reaction, depends on changes in temperature, humidity, and the contact time of the sorbent with  $SO_X$  [9]. Modeling the desulfurization process can be useful in predicting and assessing the impact of parameter changes on its efficiency, diagnosing problems, and, of course, predicting emissions under changing conditions. Modeling these elements optimizes the sulfur removal process and, in practice, serves to minimize  $SO_X$  emissions into the atmosphere. Modeling the desulfurization process can be useful in predicting and assessing the impact of parameter changes on its efficiency, diagnosing problems, and, of course, predicting emissions under changing conditions. Modeling these elements optimizes the sulfur removal process and, in practice, serves to minimize  $SO_X$  emissions into the atmosphere. The choice of the appropriate modeling method depends on the adopted goal, process scale, data availability, computing power, and time. In the literature, one can find models based on kinetic equations directly related to the calcium sorbent -  $SO_X$  reaction [10], [11] flue gas flow simulations [8], [12] and machine-learning based models [13], [14].

It is worth noting that models based on kinetic equations do not take into account the many variables affecting the desulfurization process and are difficult to implement for changing process conditions. Flow simulation requires consideration of equipment geometry, adequate knowledge, and significant computational resources. Simple regression models are easy to implement but less accurate as they do not consider the process dynamics. An alternative solution that takes all these elements into account is machine learning models. Regarding the availability of process data, the results obtained by these methods are also more realistic.

#### IV. ALGORITHM FOR CALCULATING THE IMPACT OF REAGENT INTO SO<sub>2</sub> CONCENTRATION OUTPUT

The algorithm for finding the optimal level of reagent for the  $K$ th consecutive step of the plant operation was formulated as follows:

- Set  $output_{so2}^{critical}$  critical value for SO<sub>X</sub> concentration outlet, set the number N of possible values of  $input_{ca}$  (reagent) to be examined, set the optimal  $input_{ca}^{opt}$  as  $\max\{input_{ca}(k), k = 1, 2, \dots, K - 1\}$  the maximum amount of reagent added to the system for  $k = 1, 2, \dots, K - 1$ . Denote the NARX last memory state of the depth  $d$  [ $output_{so2}(K - 1), \dots, output_{so2}(K - 5)$ ] by  $MEM^d(K - 1)$

- Train/Validate/test Narx with all samples  $k < K$
- Retrieve NARX weights and the  $meanErr$
- Set  $K$ th value of the  $input_s(K)$  of the new amount of SO<sub>2</sub> concentration inlet

- For  $i=1,2,\dots,N$  calculate the  $ANN_{output}(K) = ANN(input_{ca}(i), input_s(K), MEM^d(K - 1))$  if  $ANN_{output}(K) + meanErr < output_{so2}^{critical}$  set  $input_{ca}^{opt} = \min(input_{ca}(i), input_{ca}^{opt})$

#### V. NUMERICAL SIMULATION

##### A. NARX training and testing

The analyzed data were collected from 29.12.2019 (00:00:00) until 10.01.2020 (23:43:00) every minute. That resulted in 18706 observations; see tab.2 and fig.3.

Variable name	min	max	units
$input_{ca}$	0	1945	kg
$input_s$	0	2401	mg/Nm <sup>3</sup>
$output_{so2}$	0	1388	mg/Nm <sup>3</sup>

TABLE 2: Considered data range and units used in simulation

All the data were consecutive in time measurements. We denoted  $input_{ca}(k)$  as the  $k$ th consecutive measurement of the variable  $input_{ca}$ .

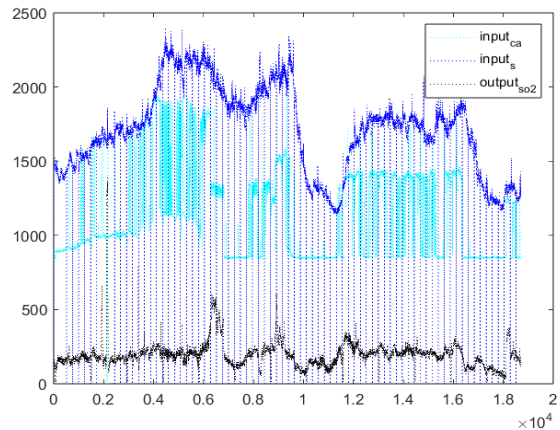


Fig. 3: Data collected from the system: SO<sub>X</sub> concentration outlet, SO<sub>X</sub> concentration inlet, reagent level

After the introductory test nonlinear 2-15-1 autoregressive exogenous Neural Network model (NARX ANN) with sigmoidal activation functions in the hidden layer and linear activation function for the output. Five ( $d=5$ ) autoregressive units were selected as the NARX memory depth.

Inputs and targets for NARX ANN were introduced as:

$$ANN_{input}(k) = \quad (6)$$

$$[input_{ca}(k), input_s, output_{so2}(k-1), \dots, output_{so2}(k-5)] \quad (7)$$

$$ANN_{target}(k) = [output_{so2}(k)] \quad (8)$$

for  $k=1,2,\dots,K-1$  ( $K=18706$ ). 70% of data was randomly taken for NARX training, 15% for validation, and the remaining 15% for testing. The NARX model was trained by three concurrent methods: Levenberg-Marquardt algorithm, Bayesian Regularization, and a scaled conjugate gradient algorithm in Matlab environment, [16], see tab. 4, 3. The obtained results for best selected NARN ANN are shown for selected data samples from the testing set, see fig. 4-7.

MSE	LM	Bayes	SCG
Training	104.59	96.67	206.29
Testing	102.03	126.86	211.34

TABLE 3: The results of NARX ANN, Mean Squared Error for training and testing sets

R	LM	Bayes	SCG
Training	0.9942	0.9949	0.9905
Testing	0.9950	0.9929	0.9867

TABLE 4: The results of NARX ANN, the correlation coefficient for training and testing sets

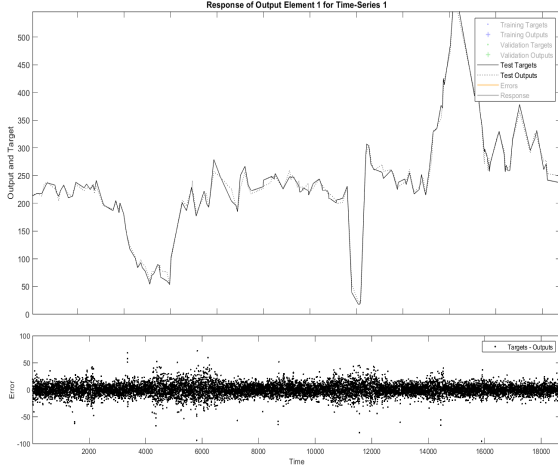


Fig. 4: Chosen results of NARX testing, predicted and measured  $SO_X$  concentration outlet level

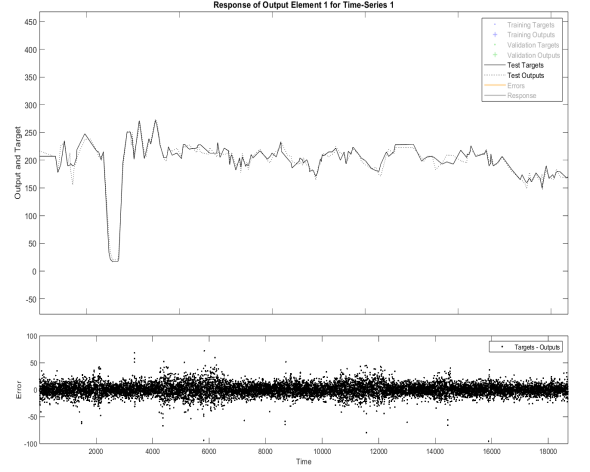


Fig. 6: Chosen results of NARX testing, predicted and measured  $SO_X$  concentration outlet level

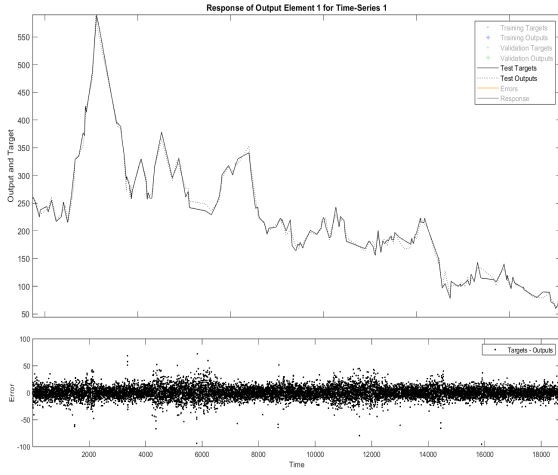


Fig. 5: Chosen results of NARX testing, predicted and measured  $SO_X$  concentration outlet level

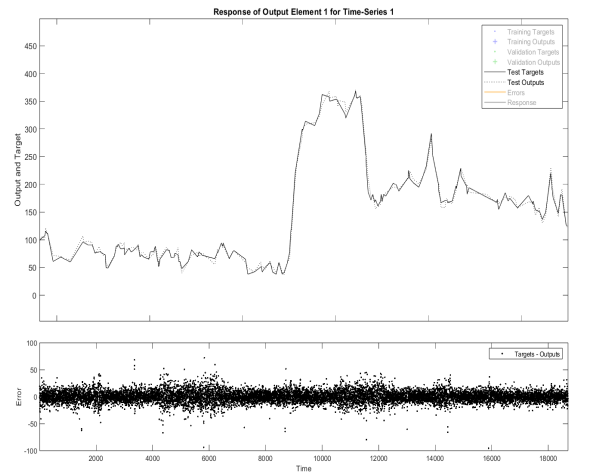


Fig. 7: Chosen results of NARX testing, predicted and measured  $SO_X$  concentration outlet level

### B. Finding the value of reagent consumption

The simulation was made as follows:

- $output_{so2}^{critical}=130$  critical value for  $SO_X$  concentration outlet,  $N=201$  of possible values of  $input_{ca}$  (reagent) to be examined, that is  $input_{ca} \in [0, 1350]$  set the optimal  $input_{ca}^{opt}$  as  $\max\{input_{ca}(k), k = 1, 2, \dots, K - 1\} = 1945$  the maximum amount of reagent added to the system for  $k = 1, 2, \dots, K - 1$ .
- Train/Validate/test Narx with all samples  $k < 18706$
- Retrieve NARX weights and the  $meanErr = 7.53$
- $input_s(18706) = 1406$  of the new amount of  $SO_X$  concentration inlet
- For  $i=1,2,\dots,201$  calculate the

$$ANN_{output}(18706) = ANN(input_{ca}(i), input_s(18706), MEM^d(18706 - 1))$$

if  $ANN_{output}(18706) + 7.5 < 130$  set

$$input_{ca}^{opt} = \min(input_{ca}(i), input_{ca}^{opt})$$

The best-selected reagent level obtained from the above simulation was 550 kg. The predicted  $SO_X$  concentration outlet for  $SO_X=1406$  for different levels of reagent in the range  $[200, 1200]$  is depicted in fig. 8. As we can see, adding more reagents results in decreasing the  $SO_X$  concentration outlet level. However, the simulation detected nonlinear behavior in the interval  $[800, 900]$  kg. The possible origins of this anomaly should be investigated in the next stage of the research. Potential causes of this in the context of the desulfurization process could be the chemical and physical properties of the reagent, process conditions (such as changes in

temperature, humidity, or flue gas flow rate), or contamination of the reagent, for example, by ash. All of these factors can affect the effectiveness of  $\text{SO}_X$  removal [17]. We have set the critical threshold at  $130 \text{ mg/Nm}^3$  because Poland is required to lower its emissions to that level by 2030. Considering the critical level 130 and taking into account the mean NARX error equals 7.5, the lowest save level of the reagent should result in  $\text{SO}_X$  concentration outlet equal  $122 \text{ mg/Nm}^3$ . For this level, the reagent level simulated by NARX ANN shows strongly decreasing behavior. Therefore the solution to the minimalization problem is singular.

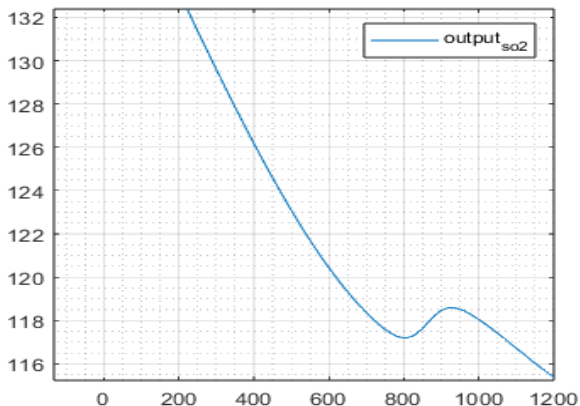


Fig. 8: Predicted  $\text{SO}_X$  concentration outlet for selected  $\text{SO}_X$  concentration inlet equal  $1406 \text{ mg/Nm}^3$  for different levels of reagent in the range  $[200, 1200] \text{ kg}$

## VI. CONCLUSIONS

In this paper, we presented data-driven modeling techniques using a nonlinear autoregressive exogenous Neural Network model. The data pertaining to the process originated from the flue gas desulfurization coal power plant.

Results indicate that:

1. NARX ANNs can therefore be used to build models of the semi-dry desulfurization process, used in practice for optimizing reagent consumption reaching in our case a coefficient of determination of up to 99% for the efficiency. In our opinion, further research should focus on optimizing the performance of NARX ANN models.
2. The obtained forecasts indicate the possibility of more efficient use of sorbent in the semi-dry desulfurization process.
3. By reducing the amount of reagent used in a process, Power Plants can save money on reagent purchases and reduce their overall water and electricity usage. This, in turn, can help to reduce the environmental impact of the process, as well as the costs associated with end product utilization. Indirectly, lower media usage decreases  $\text{CO}_2$  emissions.
4. Thanks to process optimization, coal power plants can increase their energy efficiency and reduce the costs associated with maintaining appropriate environmental

Symbol	Description
ANN	artificial neural network
NARX	autoregressive exogenous ANN
MSE	mean squared error
R	coefficient of variation
$meanErr$	mean absolute of testing errors
$input_{ca}$	reagent
$input_s$	$\text{SO}_X$ concentration inlet
$output_{so2}$	$\text{SO}_X$ concentration outlet
$output_{so2}^{critical}$	critical val. $\text{SO}_X$ concentration outlet
$k$	measurement number
$ANN_{output}(k)$	output of ANN for the $k$ input
$ANN_{target}(k)$	true value of $output_{so2}(k)$
$ANN(x)$	output of ANN for the $x$ vector input
$K - 1$	the last data used for NARX training
$d$	the depth of NARX network memory
$MEM^d(K - 1)$	$[output_{so2}(K - 1), \dots, output_{so2}(K - d)]$
$K$	the data for the control
$\text{SO}_X$	$\text{SO}_2$ and $\text{SO}_3$

TABLE 5: Nomenclature

standards. Further investigations may involve the use of other process control variables - for example, optimization of process temperature and water consumption.

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